



MAX PLANCK INSTITUTE  
FOR DYNAMICS OF COMPLEX  
TECHNICAL SYSTEMS  
MAGDEBURG



COMPUTATIONAL METHODS IN  
SYSTEMS AND CONTROL THEORY

# Reduced-order modeling for digital twins in the process industry: application to CO<sub>2</sub> methanation reactors

Luisa Peterson<sup>1</sup> Edgar Sanchez Medina<sup>1</sup> Ali Forootani<sup>3</sup>  
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November 11, 2025

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Workshop on Reduced Order and Surrogate Modeling for Digital Twins

Institute for Mathematical and Statistical Innovation, Chicago, USA, November 10 - 14, 2025

Supported by:



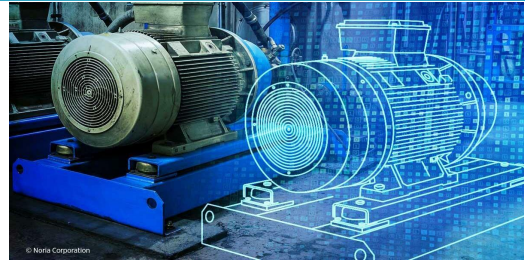
Partners:





**Digital Twins** provide a virtual model of a real-world object, device or process; they allow

- the simulation for analyzing behavior,
- optimizing design and control synthesis,
- surveillance and prediction,
- continuous improvement of the plant model and its controller.



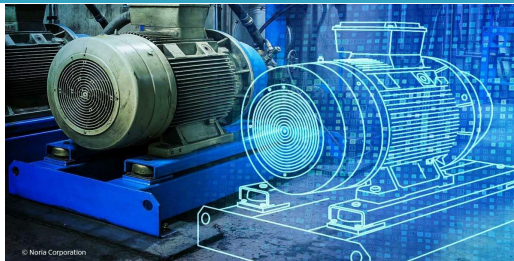
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These require real-time response times!



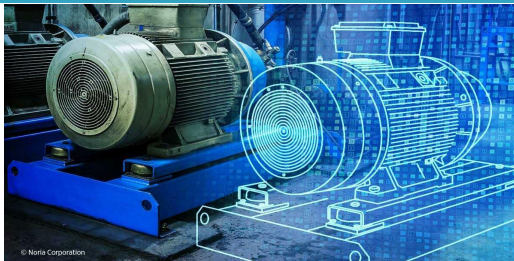
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**Smart process engineering (SmartProSys)** requires digital twins of, e.g., chemical reactors.

- This involves **mathematical models** (mass and energy balances, reaction kinetics, ...).
- For high precision, this involves accurate discretizations of systems of **nonlinear coupled partial differential equations**.
- **Real-time demands** (but also, optimization and controller design) require fast-to-evaluate surrogate models.



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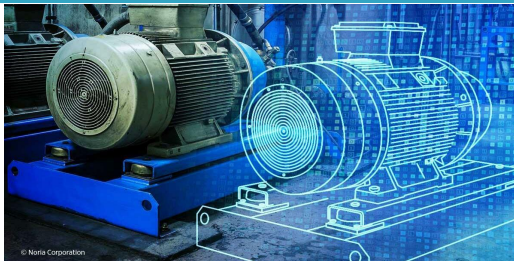




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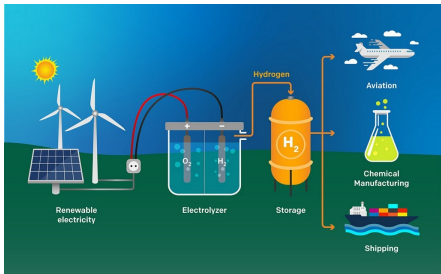
→ **MODEL REDUCTION is enabling technology!**



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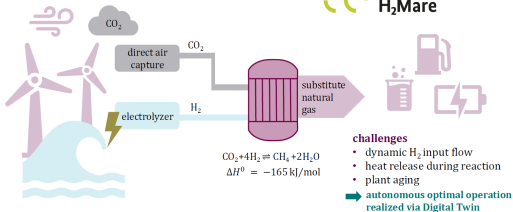
**The application  
under study**



### CO<sub>2</sub> Methanation Case Study

Rentschler et al., *Chem. Ing. Tech.* (2024)

Leitprojekt  
**H<sub>2</sub>Mare**



## What is Green Hydrogen?

- It is made from water: it is produced by splitting water into hydrogen and oxygen, and this process is called electrolysis.
- Uses clean energy: the process of electrolysis is powered by renewable energy sources like solar and wind energy.

## How does Green Hydrogen work?

- Electrolysis: electricity from renewable sources is used to power a device (an electrolyzer).
- Collecting: the gas is then collected and can be stored or transported to where it's needed.
- Using Hydrogen: it can then be used as a fuel (the only byproduct is water) or in reaction with carbon dioxide.



## The long-term goal and some of our works

- The **goal** of our project is the development of a **Digital Twin** for a [methanation reactor](#).
- Such a reactor is used to **convert renewable hydrogen** (coming from electrolysis) to more easily-distributable methane.



## The long-term goal and some of our works

- The **goal** of our project is the development of a **Digital Twin** for a [methanation reactor](#).
- Such a reactor is used to **convert renewable hydrogen** (coming from electrolysis) to more easily-distributable methane.
- For this purpose, we study a *tubular catalytic wall reactor* and a **semi-discretized dynamic model constructed by mass and energy balances**; preliminary works are listed below ↓



Reactor for the catalytic CO<sub>2</sub> methanation

- I. V. G., L. Peterson, P. Goyal, J. Bremer, K. Sundmacher, and P. B.: *Learning reduced-order Quadratic-Linear models in Process Engineering using Operator Inference*, ENUMATH 2023 Proceedings.
- L. Peterson, A. Forootani, E. Sanchez Medina, I. V. G., K. Sundmacher, and P. Benner: *Towards Digital Twins for Power-to-X: Comparing Surrogate Models for a Catalytic CO<sub>2</sub> Methanation Reactor*, 2024.
- L. Peterson, L., M. Büttner, A. Forootani, I. V. G., P. Benner, and K. Sundmacher: *Greedy Sampling Neural Network SINDy with Control for a Catalytic CO<sub>2</sub> Methanation Reactor*, LSSC 2025 Proceedings.



- The synthetic data are generated from a first-principles reactor model adapted to a pilot plant setting.
- Specifically, we use a one-dimensional polytropic reactor model to generate synthetic data.

## Mechanistic Reactor Model

Zimmermann et al., *Chem. Eng. J.* (2022)

### reaction rate

$$\sigma_{\text{eff}} = \eta \sigma_{\text{int}}$$

$$\sigma_{\text{int}} = k p_{\text{CO}_2}^{n_{\text{CO}_2}} p_{\text{H}_2}^{n_{\text{H}_2}} \left( 1 - \frac{p_{\text{CH}_4} p_{\text{H}_2\text{O}}^2}{K_{\text{eq}} p_{\text{CO}_2} p_{\text{H}_2}^4} \right)$$

$$k = k_{0,\text{ref}} \exp \left( \frac{E_A}{R} \left( \frac{1}{T_{\text{ref}}} - \frac{1}{T} \right) \right)$$

**mass balance:**  $\varepsilon \frac{\partial c_i}{\partial t} = -\vec{u} \cdot \nabla c_i + \nabla (D_i^{\text{eff}} \nabla c_i) + (1 - \varepsilon) v_i \sigma_{\text{eff}}$

**energy balance:**  $(\rho c_p)_{\text{eff}} \frac{\partial T}{\partial t} = -(\rho c_p)_{\text{fluid}} \vec{u} \cdot \nabla T + \nabla \cdot (\Lambda_{\text{eff}} \nabla T) + (1 - \varepsilon) (-\Delta H_R) \sigma_{\text{eff}}$

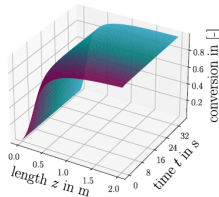
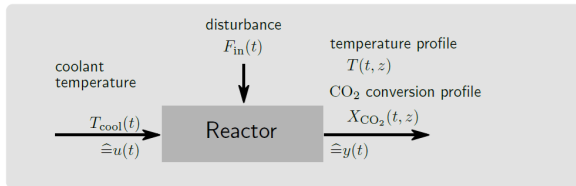
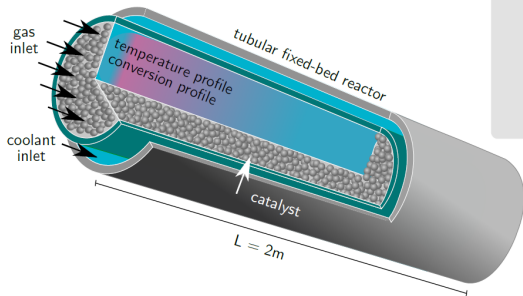
### assumptions and details

- one- & two-dimensional model
- parameters fitted to experimental data
- discretized via finite volume method
- integrated by use of Kvaerno5 solver (within the diffrax library)

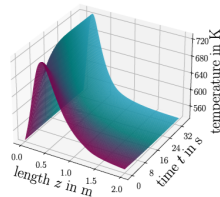
### challenges

- nested parameter dependencies
- non-linearities  $\rightarrow$  high disturbance sensitivity
- dynamics on different scales  $\rightarrow$  stiff
- model solutions involve many states (after semi-discretization)

- Reaction kinetics and heat transfer parameters are calibrated against steady-state experimental data from a pilot plant.



$\text{CO}_2$  conversion profile



temperature profile





**The proposed  
methods**

# SciML and surrogate modeling through stable Operator Inference (OpInf) <sup>★</sup> and GN-SINDy <sup>★</sup>

- The results presented in what follows were published this year in the IEEE Transactions on Automation Science and Engineering (free copy available on TechRxiv):

L. Peterson et al., *Towards Digital Twins for Power-to-X: Comparing Surrogate Models for a Catalytic CO<sub>2</sub> Methanation Reactor*, 2025



Towards Digital Twins for Power-to-X Processes  
Comparing Surrogate Models for a  
Catalytic CO<sub>2</sub> Methanation Reactor

Laura Peterson<sup>1</sup>, Ali Pourzand<sup>2</sup>, Senior Member IEEE, Edgar Ivan Sanchez Medina<sup>3</sup>, Jon Victor Gomez Kai Soudbracker<sup>4</sup>, and Bruce Bonnor<sup>5</sup>

[illegible]

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**T**HE global effort to combat climate change requires a transition to renewable energy sources. The *Power-to-X* concept plays a central role in this effort by facilitating the conversion of renewable energy (e.g., from solar power or wind) to readily distributable chemical energy carriers. One of the processes within this framework is the catalytic methanation of carbon dioxide (CO<sub>2</sub>) with green hydrogen (H<sub>2</sub>) produced by electrolysis, enabling the storage of renewable energy.

As shown below, the catalytic CO<sub>2</sub> methanation process converts carbon dioxide and hydrogen into methane and water:

$$\text{CO}_2 + 4 \text{H}_2 \rightarrow \text{CH}_4 + 2 \text{H}_2\text{O}$$

Traditionally, this conversion takes place in a fixed reactor that is either packed with catalyst particles or has a catalyst coated on its inner wall.

$$\text{CH}_3 + \text{H}_2 \rightarrow \text{CH}_4 + \text{H} \cdot$$

[illegible]

To address the computational limitations of mechanistic models, we employ surrogate models, simplified representations that capture the essential system dynamics, while significantly reducing computational time [31], [32]. They generally fall into three main categories: (1) (i).

- ★ P. Goyal, I. Pontes Duff, P. Benner, *Guaranteed Stable Quadratic Models and their applications in SINDy and Operator Inference*, Physica D: Nonlinear Phenomena, Vol. 483, pp. 134893, 2025.

- \* A. Forootani, P. Benner, *GN-SINDy: Greedy Sampling Neural Network in Sparse Identification of Nonlinear Partial Differential Equations*, arXiv:2405.08613. 2024.



# Reduced-Order Model: Operator Inference

Peherstorfer & Willcox, *Comp. Meth. Appl. Mech. Eng.* (2016); Goyal et al., *Phys. D* (2025)

1

principal component analysis + projection

a) PCA via SVD

$$\begin{array}{c} \mathbf{Q} \\ n \times d \end{array} = \begin{array}{c} \mathbf{U}_r \\ n \times r \end{array} \begin{array}{c} \mathbf{\Sigma}_r \\ r \times r \end{array} \begin{array}{c} \mathbf{V}_r^T \\ r \times d \end{array}$$

$$\begin{array}{c} \mathbf{U} \\ n \times n \end{array} \quad \begin{array}{c} \mathbf{\Sigma} \\ n \times d \end{array} \quad \begin{array}{c} \mathbf{V}^T \\ d \times d \end{array}$$

b) projection on low dimensional basis

$$\begin{array}{ccc} \mathbf{Q} & \xrightarrow{\cdot \mathbf{U}_r^T} & \hat{\mathbf{Q}} \\ \dot{\mathbf{Q}} & \xrightarrow{\cdot \mathbf{U}_r^T} & \dot{\hat{\mathbf{Q}}} \end{array} \quad \begin{array}{ccc} \hat{\mathbf{Q}} & \xrightarrow{\cdot \mathbf{U}_r} & \tilde{\mathbf{Q}} \\ \dot{\hat{\mathbf{Q}}} & \xrightarrow{\cdot \mathbf{U}_r} & \dot{\tilde{\mathbf{Q}}} \end{array}$$

compress      decompress

2

low-dimensional regression

a) define reduced-order model structure

$$\dot{\hat{\mathbf{q}}} = \hat{\mathbf{A}}\hat{\mathbf{q}} + \hat{\mathbf{H}}(\hat{\mathbf{q}} \otimes \hat{\mathbf{q}}) + \hat{\mathbf{B}}\mathbf{u}$$

b) get reduced operators

$$\min_{\hat{\mathbf{A}}, \hat{\mathbf{H}}} \left\| \hat{\mathbf{Q}}^T \hat{\mathbf{A}}^T + (\hat{\mathbf{Q}} \odot \hat{\mathbf{Q}})^T \hat{\mathbf{H}}^T + \mathbf{U}^T \hat{\mathbf{B}}^T - \dot{\hat{\mathbf{Q}}}^T \right\|_F^2$$

solve with **gradient-based optimization**

**stable OpInf:** choose a parameterization of  $\hat{\mathbf{A}}$  and  $\hat{\mathbf{H}}$ , such that the inferred models are stable by design



Asymptotic (exponential, Lyapunov) stability of linear systems

$$\dot{x}(t) = Ax(t), \quad x(0) = x_0,$$

can be explicitly parameterized:

### Theorem (Gillis/Sharma 2017)

*A matrix  $A \in \mathbb{R}^{n \times n}$  is asymptotically stable (Hurwitz, Lyapunov stable) if and only if it can be represented as*

$$A = (J - R)Q,$$

*where  $J = -J^T$  and  $R = R^T$ ,  $Q = Q^T$  are both positive definite.*

$\implies$  **Stability-preserving Oplnf for linear systems:**

$$(S_*, L_*, K_*) := \underset{\substack{L, K \text{ upper triangular} \\ \text{with positive diagonals}}}{\operatorname{argmin}} \left( \|\dot{X} - (S - S^T - L^T L)K^T K X\|_F^2 + \mathcal{R}(L, K, S) \right)$$

The matrix obtained from this **nonlinear (regularized) least-squares problem**,

$$A_* = \left( S_* - S_*^T - L_*^T L_* \right) K_*^T K_*,$$

is guaranteed to be stable due to [GILLIS/SARMA 2017]. Related work by Schwerdtner, Voigt, ...

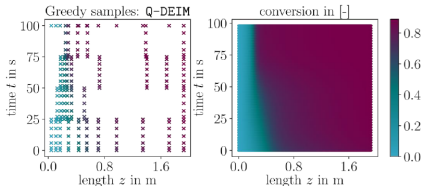


# Reduced-Order Model: Greedy Sparse Identification

Brunton et al., *Proc. Natl. Acad. Sci.* (2016), Forootani & Benner, *arXiv* (2024)

1

greedy sampling via Q-DEIM



- a) **POD** to construct a reduced approximation of the snapshot matrix
- b) **QR DECOMPOSITION** with column pivoting to select key time and space indices from reduced matrices

2

sparse regression on a library

$$\mathcal{L} = \text{MSE}(u, \hat{u}) + \text{MSE}(\hat{u}_t, \theta \tilde{\xi}) + L_1(\tilde{\xi})$$



$$(z, t) \longrightarrow \hat{u} \in \{\hat{X}, \hat{T}\}$$

Auto. Diff.  
↔  
Include in  $\mathcal{L}$

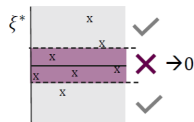
$$\hat{u}_t = \theta \tilde{\xi}^T$$

$$\begin{bmatrix} \partial_t \hat{u} \end{bmatrix} = \begin{bmatrix} u \\ u_z \\ uu_z \\ \vdots \\ u^2 u_{zz} \\ \vdots \end{bmatrix} \begin{bmatrix} \tilde{\xi} \end{bmatrix}$$

Library

Normalize

$$\xi^* = \xi \cdot \frac{\|\theta\|}{\|u_t\|}$$





The GN-SINDy approach introduces several **improvements to standard SINDy**:

- In step (a) of GN-SINDy, the Q-DEIM algorithm is used to sample the data set.
  - Q-DEIM first applies the SVD to extract dominant features by retaining singular values above a precision threshold  $\epsilon_{\text{tresh}}$  (linked to DEIM\_tolerance), then uses QR decomposition with pivoting to select key spatio-temporal indices.
  - This sensor placement strategy efficiently balances the trade-off between preserving essential dynamics and computational cost.
- 
- In step (b), sample pairs  $(t_i, x_i)$  from Q-DEIM are entered into a DNN.
  - The DNN learns the nonlinear mapping  $(t, x) \mapsto u$  and the underlying physics via  $\frac{\partial u}{\partial t} = \theta \xi$ .
  - The output  $\hat{u}$  of the DNN serves as a function approximation used to construct the dictionary  $\Theta$  and compute  $\frac{\partial \hat{u}}{\partial t}$  by automatic differentiation.

- Step (c) estimates  $\xi$  via stochastic gradient descent to minimize the loss function.
- The loss function for training the DNN comprises of a MSE component to capture the mapping  $(t, x) \rightarrow \hat{\mathbf{u}}$ , and an additional term to enforce constraints on the DNN solutions:

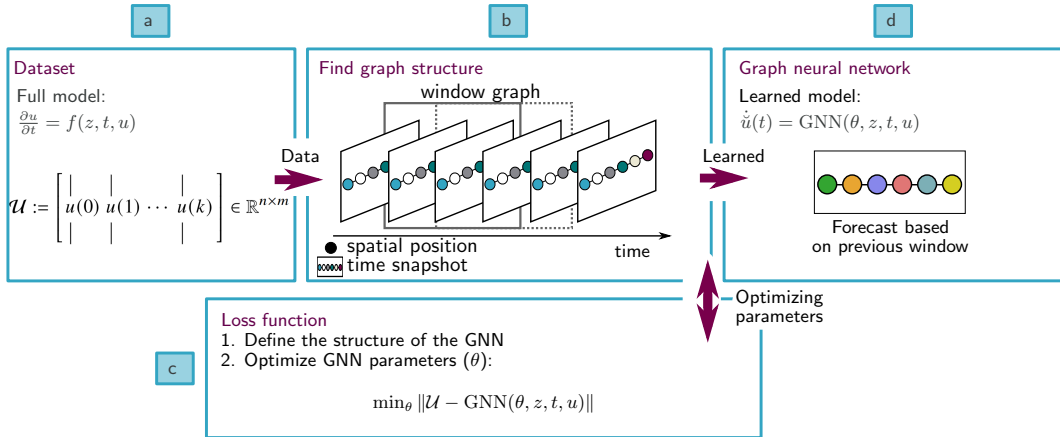
$$\mathcal{L} = \frac{1}{\mathcal{N}} \sum_{i=1}^{\mathcal{N}} \left( \mathbf{u}(t_i, x_i) - \hat{\mathbf{u}}(t_i, x_i) \right)^2 + \frac{1}{\mathcal{N}} \sum_{i=1}^{\mathcal{N}} \left( \frac{\partial \hat{\mathbf{u}}(t_i, x_i)}{\partial t_i} - \Theta(\hat{\mathbf{u}}(t_i, x_i))(\xi \odot \mathbf{g}) \right)^2.$$

- $(t_i, x_i)$  are the selected sample pairs in the domain,  $\mathbf{u}(t_i, x_i)$  is calculated using the Q-DEIM algorithm applied to the snapshot matrix  $\mathcal{U}$  and  $\mathbf{g}$  is the sparsity mask.
- The DNN is constrained by the element-wise multiplication of  $\xi$  and  $\mathbf{g}$ , not by  $\xi$  alone.
- In step (d), the learned coefficient vector yields a model explaining the original data set.

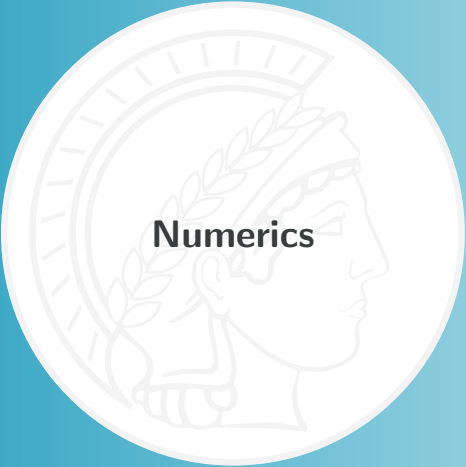
↪ see also the work in [Forootani et al. '24] (arXiv:2405.08613).

# Comparison method: GNN (GAT)

- GATs use attention mechanisms to assign adaptive weights to neighbors based on their relevance, making them effective for tasks where the importance of neighboring nodes varies significantly [Veličković et al. '18];





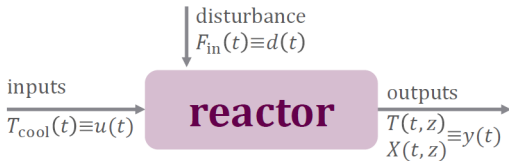


# Numerics



# Comparative Analysis – Study Design

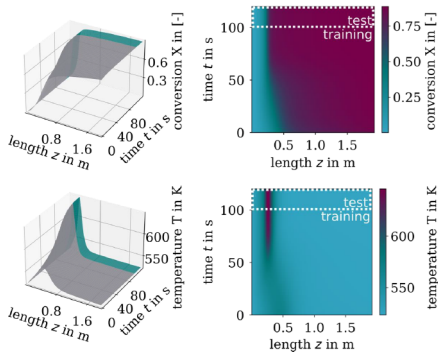
Peterson et al., *IEEE Trans. Autom. Sci. Eng.* (2025)



scenario (i):  $F_{in}(t)$  ↓  
scenario (ii):  $F_{in}(t)$  ↑  
scenario (iii):  $T_{cool}(t)$  ↓  
scenario (iv):  $T_{cool}(t)$  ↑

- get data based on the mechanistic model
- train on the first ~80 % of the time trajectory, **predict** the remaining ~20 %
- run each model **10×** for each scenario

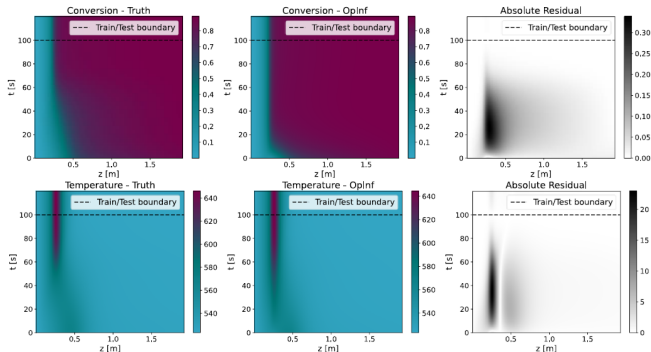
trajectories for scenario (i)





# Operator Inference - Results

Peterson et al., *IEEE Trans. Autom. Sci. Eng.* (2025)



results for  
scenario (i)

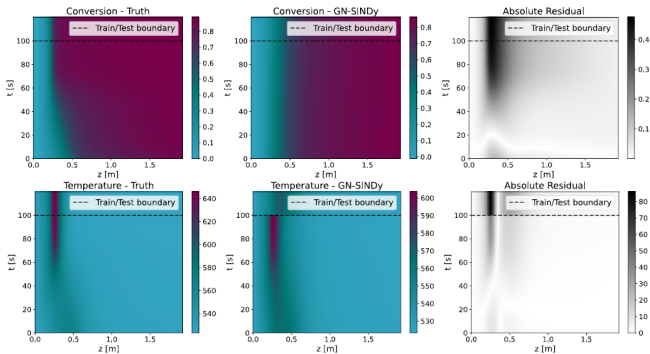
forecasting  
speedup factor:  
10.66

| test (i)             | test (ii)            | test (iii)          | test (iv)           | training time            | forecasting time          | input parameter | model parameter |
|----------------------|----------------------|---------------------|---------------------|--------------------------|---------------------------|-----------------|-----------------|
| $0.067 \pm 0.046 \%$ | $0.075 \pm 0.059 \%$ | $0.25 \pm 0.010 \%$ | $0.30 \pm 0.018 \%$ | $2816 \pm 366 \text{ s}$ | $0.64 \pm 0.15 \text{ s}$ | 6               | 42              |



# Greedy Sparse Identification - Results

Peterson et al., *IEEE Trans. Autom. Sci. Eng.* (2025)



results for  
scenario (i)

forecasting  
speedup factor:  
48.71

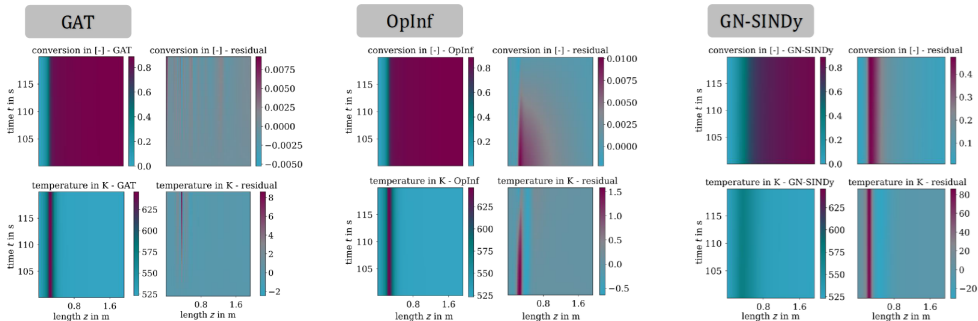
| test (i)            | test (ii)            | test (iii)          | test (iv)           | training time         | forecasting time           | input parameter | model parameter |
|---------------------|----------------------|---------------------|---------------------|-----------------------|----------------------------|-----------------|-----------------|
| $3.78 \pm 0.018 \%$ | $1.09 \pm 0.0080 \%$ | $6.47 \pm 0.070 \%$ | $6.31 \pm 0.069 \%$ | $96 \pm 49 \text{ s}$ | $0.14 \pm 0.012 \text{ s}$ | 792 – 1438      | 13186           |



# Comparative Analysis – Prediction Error

Peterson et al., *TechRxiv* (2024)

prediction results  
for scenario (i)

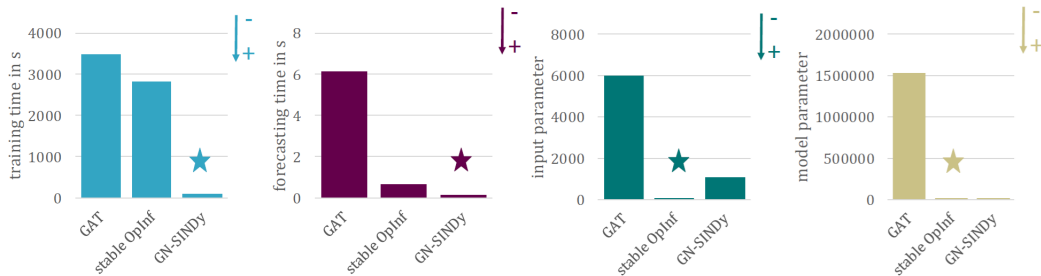


| method       | test (i)             | test (ii)            | test (iii)          | test (iv)           |
|--------------|----------------------|----------------------|---------------------|---------------------|
| GAT          | $0.17 \pm 0.075 \%$  | $0.097 \pm 0.059 \%$ | $0.29 \pm 0.033 \%$ | $0.21 \pm 0.030 \%$ |
| Stable OpInf | $0.067 \pm 0.046 \%$ | $0.075 \pm 0.059 \%$ | $0.25 \pm 0.010 \%$ | $0.30 \pm 0.018 \%$ |
| GN-SINDy     | $3.78 \pm 0.018 \%$  | $1.09 \pm 0.0080 \%$ | $6.47 \pm 0.070 \%$ | $6.31 \pm 0.069 \%$ |



# Comparative Analysis – Complexity

Peterson et al., *TechRxiv* (2024)



| method       | training time | forecasting time | input parameter | model parameter |
|--------------|---------------|------------------|-----------------|-----------------|
| GAT          | 3475 ± 213 s  | 6.11 ± 0.039 s   | 6000            | 1528130         |
| Stable OpInf | 2816 ± 366 s  | 0.64 ± 0.15 s    | 6               | 42              |
| GN-SINDy     | 96 ± 49 s     | 0.14 ± 0.012 s   | 792 – 1438      | 13186           |



## Summary & Outlook

### why Digital Twin?

- concept that **bi-directionally** links a physical entity to a model
- goal: enable **optimal control** for PtX
- **real-time** model execution needed



### what we did

- compared three surrogate models:
  - Spatio-Temporal Neural Networks (**ST-NN**),
  - Greedy Sparse Identification (**GN-SINDy**),
  - Operator Inference (**OpInf**)
- focus: speed, accuracy, and generalizability



### key findings

|          | ST-NN | GN-SIN<br>Dy | OpInf |
|----------|-------|--------------|-------|
| accuracy | ✓     |              | ✓     |
| speed    |       | ✓            | ✓     |



### next steps

- **closed-loop control** integration
- Analysis of other **ROM methods**
- Full **Digital Twin** implementation



Special thanks also to Pawan Goyal (appliedAI Initiative GmbH), Jens Bremer (TU Clausthal), Ronny Zimmermann & Alexander Geschke (MPI, PSE), Miriam Büttner (TU Berlin) ...



Our recent survey paper (one of the first **Digital Twin** survey in **Process Engineering**), addresses the following relevant topics\*:

- **Guidance for practitioners:** Providing guidance to researchers and practitioners in **Process Engineering** and chemical engineering fields.
- **Real-time representation:** Addressing real-time representation challenges in **Digital Twin** development and offering practical solutions.
- **Numerical methods review:** Comprehensive review of state-of-the-art numerical methods and tools for constructing **Digital Twins**, with a focus on applications in **Process Engineering**.
- **Unlocking potential:** Highlighting the transformative potential of **Digital Twins** in **Process Engineering** and offering insights into essential mathematical tools to be harnessed.

\* L. Peterson, I. V. G., P. Benner and K. Sundmacher: *Digital twins in process engineering: An overview on computational and numerical methods*, Computers & Chemical Engineering, Vol. 193, pp. 108917, February, 2025.





CSC

COMPUTATIONAL METHODS IN  
SYSTEMS AND CONTROL THEORY

## The team behind it

GEFÖRDERT VOM



Bundesministerium  
für Bildung  
und Forschung



Leitprojekt  
**H<sub>2</sub>Mare**



SmartProSys



# Thank you for your attention!



Peterson et al., IEEE Trans.  
Autom. Sci. Eng. (2025)



Peterson et al., Comput.  
Chem. Eng. (2025)



# **Bibliography**



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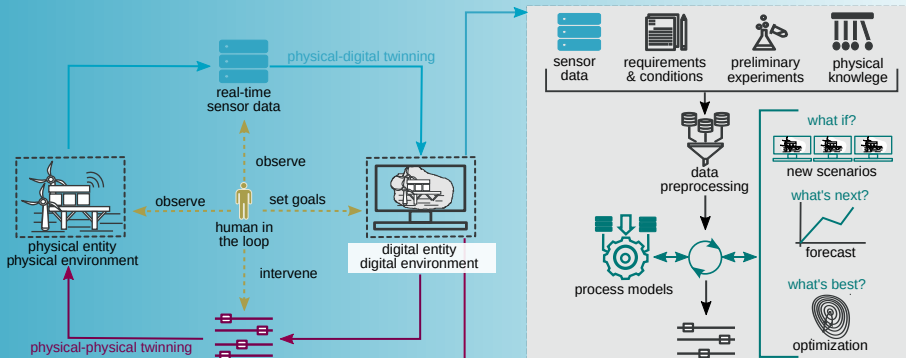
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**Thank you!**  
**Any questions?**



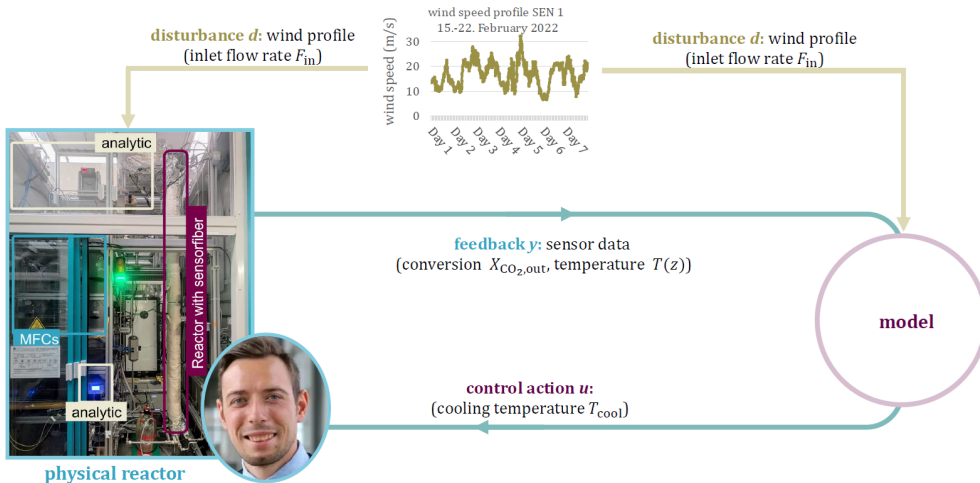
## The twinning scenario

- Real-time sensor data and physical models of an existing chemical plant (the physical entity), are used to represent its current state as a virtual entity.
- This virtual entity can provide several benefits, e.g., scenario exploration, prediction, and optimization.
- The virtual and physical entities are thus connected in real time through bi-directional data exchange.





# Digital Twin Data Flow





- The energy balance equation describes the energy distribution in the reactor, taking into account heat conduction, convective heat transport, heat exchange with the environment.

$$(\rho c_p)_{\text{eff}} \frac{\partial T}{\partial t} = -u_{\text{in}} \rho_{\text{in}} c_p \frac{\partial T}{\partial z} + \frac{\partial}{\partial z} \left[ \Lambda_z \frac{\partial T}{\partial z} \right] - \frac{4U}{D} (T - T_{\text{cool}}) - \Delta H_r (1 - \varepsilon_R) \zeta \sigma_{\text{eff}}$$

- Each term represents a specific aspect of heat transport and heat reaction in the reactor:
  1.  $(\rho c_p)_{\text{eff}} \frac{\partial T}{\partial t}$ : indicates how quickly the temperature in the reactor changes over time. It depends on the reactor's effective heat capacity, which is determined by the reactor's material.
  2.  $-u_{\text{in}} \rho_{\text{in}} c_p \frac{\partial T}{\partial z}$ : reflects the influence of convective heat transport along the reactor axis.
  3.  $\frac{4U}{D} (T - T_{\text{cool}})$ : represents the heat loss due to heat transfer at the wall of the reactor.
  4.  $-\Delta H_r (1 - \varepsilon_R) \zeta \sigma_{\text{eff}}$ : takes into account the heat released/absorbed due to the chemical reaction.



- The resulting mass balance equation for the conversion of  $\text{CO}_2$  is:

$$\varepsilon_R \frac{\partial X}{\partial t} = -u \frac{\partial X}{\partial z} + \frac{M_{\text{CO}_2}}{\rho y_{\text{CO}_2, \text{in}}} (1 - \varepsilon_R) \zeta \sigma_{\text{eff}} \quad (1)$$

with the following terms:

1.  $\varepsilon_R \frac{\partial X}{\partial t}$ : reflects how quickly the conversion of  $\text{CO}_2$  in the reactor changes over time.
2.  $-u \frac{\partial X}{\partial z}$ : describes the influence of the flow velocity on the spatial distribution of the  $\text{CO}_2$  conversion in the reactor (convective transport in the z-direction).
3.  $\frac{M_{\text{CO}_2}}{\rho y_{\text{CO}_2, \text{in}}} (1 - \varepsilon_R) \zeta \sigma_{\text{eff}}$ : encompasses the chemical reaction itself, where  $\sigma_{\text{eff}}$  represents the effective reaction rate.





- Taking into account the conversion law for mass and energy, for any control volume of different shape and size within the reactor, the following basic set of equilibrium equations (Euler specification) applies:

$$\text{Totale Masse } \frac{\partial \rho}{\partial t} = -\nabla \cdot (\rho \vec{u}) \quad (2)$$

$$\text{Komponenten Masse } \rho \frac{\partial \omega_\alpha}{\partial t} = -\rho \vec{u} \nabla \cdot \omega_\alpha - \nabla \cdot \vec{j}_\alpha + M_\alpha \sum_\beta \nu_{\alpha,\beta} \tilde{r}_\beta \quad (3)$$

$$\text{Energie } \rho c_p \frac{\partial T}{\partial t} = -\rho c_p \vec{u} \nabla T - \nabla \cdot \vec{q} - \sum_\beta \nu_{\alpha,\beta} \left( \Delta_R \tilde{H}_\beta \right) \tilde{r}_\beta \quad (4)$$

- When considering a single reaction, the mass balance equation of the components  $\text{CO}_2$ ,  $\text{H}_2$ ,  $\text{CH}_4$ ,  $\text{H}_2\text{O}$  and  $\text{N}_2$  can be summarized in a single equation by using the carbon dioxide conversion  $X_{\text{CO}_2}$ :

$$\dot{n}_i = \dot{n}_{i,\text{in}} + \nu_i X_{\text{CO}_2} \dot{n}_{\text{CO}_2,\text{in}} \quad (5)$$